

Thin Film Simulation on a Rotating Wafer



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... your problems flow to a solution!

- **Motivation**
- **Finite Area Method**
- **Thin Film Model**
- **Impinging Jet**
- **Polydual Mesh**
- **Comparison with 3D Solution**
- **Conclusion**
- **Outlook & Discussion**

- **Our industry partner, LAM Research AG, initiated a project to be able to optimize their product, a spin processor**
 - One-sided single wafer wet processing
 - Patented wafer chuck with floating wafer (N₂ cushion)
 - Vertically arranged process levels
 - Clearly separated chemical lines



- **2D Simulation
(Axial-Symmetric)**

- Advantages

- Reasonably small meshes
- Short computation times in order of hours
- No additional model assumptions

- Disadvantages

- Allows only central impingement
- Resolve waves only in radial direction

- **3D Simulation**

- Advantages

- Fine resolution only where required
- No additional model assumptions

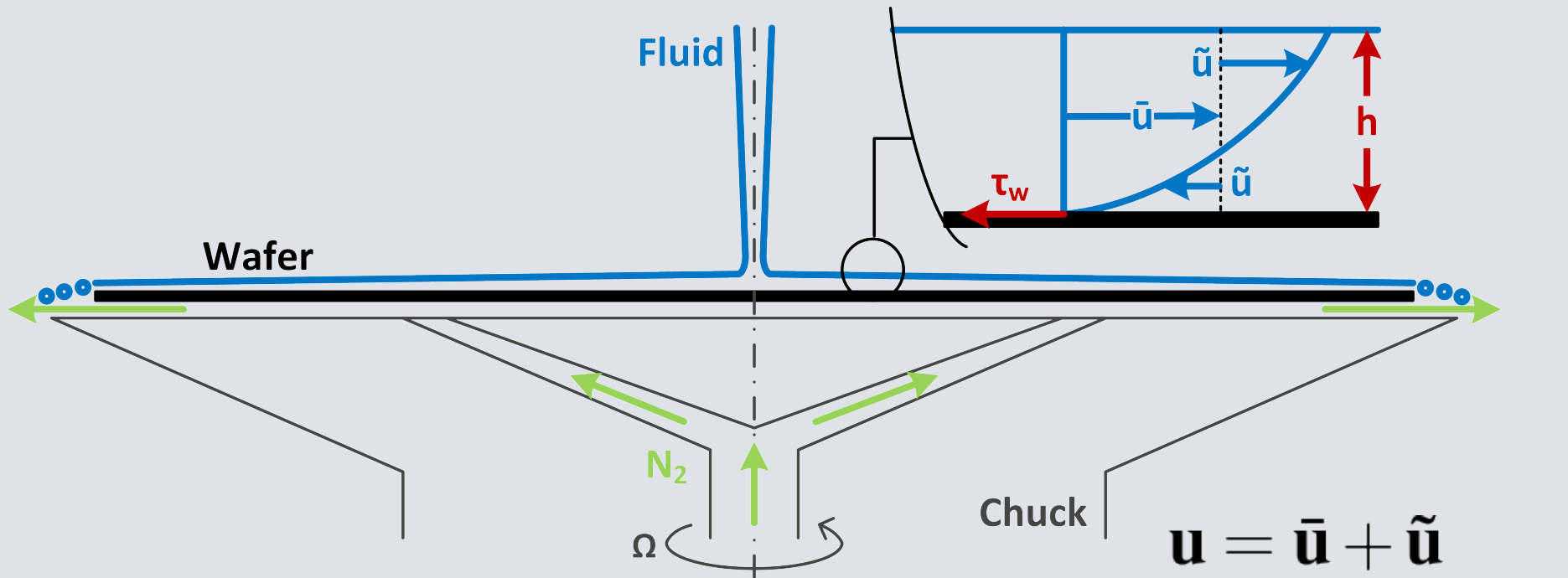
- Disadvantages

- Huge meshes
 - Still cannot fully resolve all physical aspects
- Long computation times in order of weeks/months

- **Specialization of FVM to flows on surfaces-films**
- **Implementation by H. Jasak and Z. Tukovic in OpenFOAM-ext project**
 - Only present in 1.5-dev and 1.6-ext version
- **Demonstration solver models the transport equation on a prescribed velocity field**
 - `surfactantFoam` solver
- **Equations are solved on a boundary patch of the volume mesh**
 - FV-solution can be used as a source term

- **Normal velocity component is negligible compared to tangential one**
- **Pressure is constant across the film thickness**
- **Laminar flow**
- **Film thickness is identical with a velocity boundary layer**
- **Parabolic velocity profile assumed across the film thickness**

Thin Film Model (2)



- **Dependent variables**

- Film thickness h
- Mean velocity \bar{u}

$$\mathbf{u} = \bar{\mathbf{u}} + \tilde{\mathbf{u}}$$

$$\bar{\mathbf{u}} = \frac{1}{h} \int_h \mathbf{u} dx_3$$

- **Continuity Equation**

$$\frac{\partial}{\partial t} h + \nabla (h\bar{\mathbf{u}}) = 0$$

- **Momentum Equation**

$$\begin{aligned} \frac{\partial}{\partial t} (h\bar{\mathbf{u}}) + \nabla (h\bar{\mathbf{u}}\bar{\mathbf{u}}) + \nabla \left(\int_h \tilde{\mathbf{u}}\tilde{\mathbf{u}} dx_3 \right) \\ = -\frac{1}{\rho} h \nabla p + \frac{1}{\rho} (-\tau_{\text{wafer}}) \end{aligned}$$

- where the pressure is expressed by

$$p = \rho |\mathbf{g}| h - \sigma \kappa$$

- with a surface curvature approximated by

$$\kappa \approx \nabla^2 h$$

- and shear stress at wafer is described by

$$\tau_{\text{wafer}} = \mu \left. \frac{\partial}{\partial x_3} \mathbf{u} \right|_{x_3=0}$$

- In order to describe the shear stress at the wafer and the differential advection, we introduce a polynomial velocity profile function

$$u(\xi) = \mathbf{a}_0 + \mathbf{a}_1\xi + \mathbf{a}_2\xi^2 + \mathbf{a}_3\xi^3$$
$$\xi \in \langle 0, 1 \rangle, x_3 = h\xi$$

- which defines the free surface velocity

$$\mathbf{u}_{\text{fs}} = u(\xi) \Big|_{\xi=1}$$

- and fulfils following boundary conditions

$$\int_0^1 u(\xi) d\xi = \bar{u}$$

$$u(\xi) \Big|_{\xi=0} = \mathbf{u}_{\text{wafer}}$$

$$\frac{\partial^2}{\partial \xi^2} u(\xi) \Big|_{\xi=0} = 0$$

$$\frac{\partial}{\partial \xi} u(\xi) \Big|_{\xi=1} = 0$$

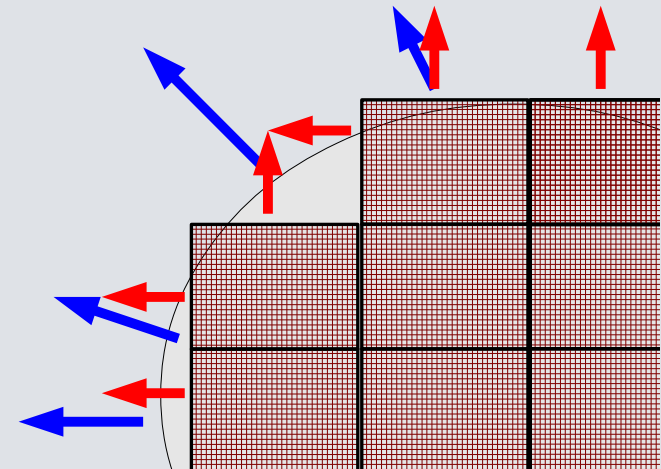
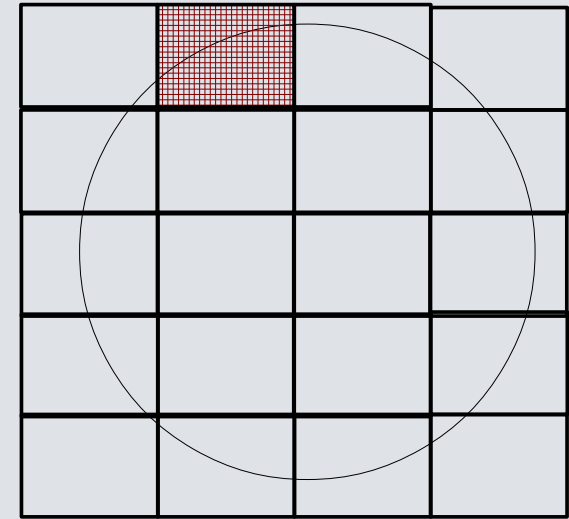
- The boundary conditions imposed on the velocity profile function lead to the following solutions

$$\begin{aligned}\nabla \left(\int_h \tilde{\mathbf{u}} \tilde{\mathbf{u}} dx_3 \right) &= \nabla \left[\int_0^1 (u(\xi) - \bar{\mathbf{u}}) (u(\xi) - \bar{\mathbf{u}}) h d\xi \right] \\ &= \nabla \left[\frac{213}{875} h (\bar{\mathbf{u}} - \mathbf{u}_{\text{wafer}}) (\bar{\mathbf{u}} - \mathbf{u}_{\text{wafer}}) \right]\end{aligned}$$

$$\begin{aligned}\tau_{\text{wafer}} &= \mu \left. \frac{\partial}{\partial (h\xi)} u(\xi) \right|_{\xi=0} \\ &= \mu \frac{1}{h} \frac{12}{5} (\bar{\mathbf{u}} - \mathbf{u}_{\text{wafer}})\end{aligned}$$

- **Impingement area is generally not known**
 - Impinging jet is moving over the wafer
- **Thin film model is not valid in the impingement area and its surrounding**
 - Solution in the impingement area is known from FVM
 - Impingement area is “weakly” influenced from “outside”
- **Possible impingement implementations**
 - Remeshing
 - Impingement area is represented by a circular boundary condition which moves and the mesh is adapted
 - Fixation of solution in faces
 - Impingement faces are selected and solution is prescribed

- **Fixation of solution in the faces has significant advantages over remeshing, however it has its own problems**
 - “Crown Cap” effect
 - Faces in the impingement area are not resolving exact circle
 - Face boundaries are not aligned with a circle
 - Total mass-flow correction
 - Inlet velocity profiles
 - Velocities varies along the jet edge

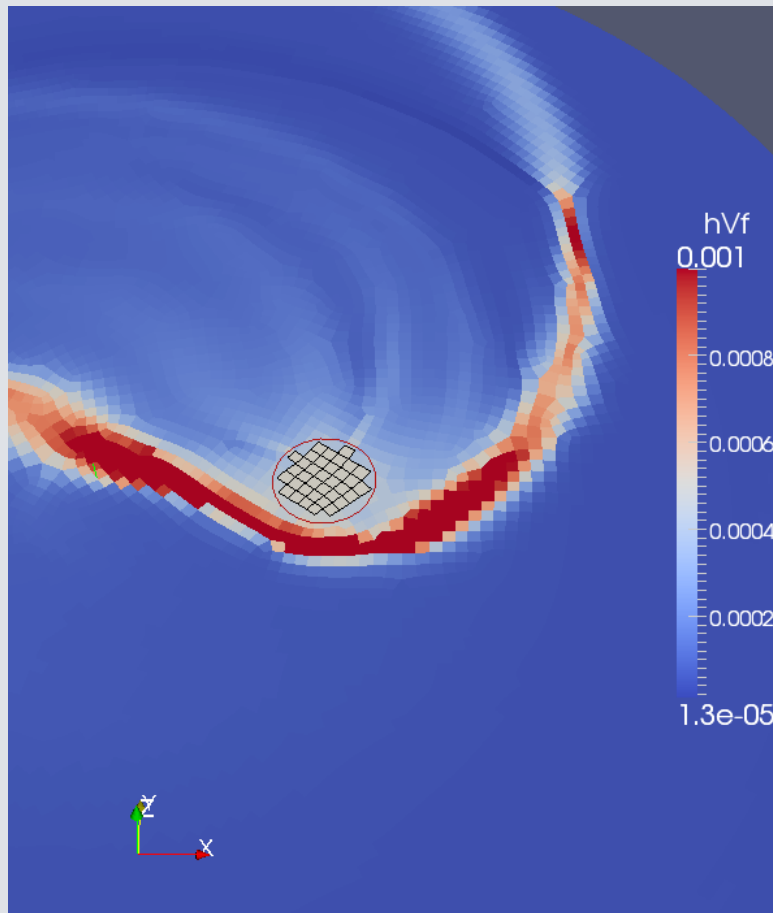


... your problems flow to a solution!

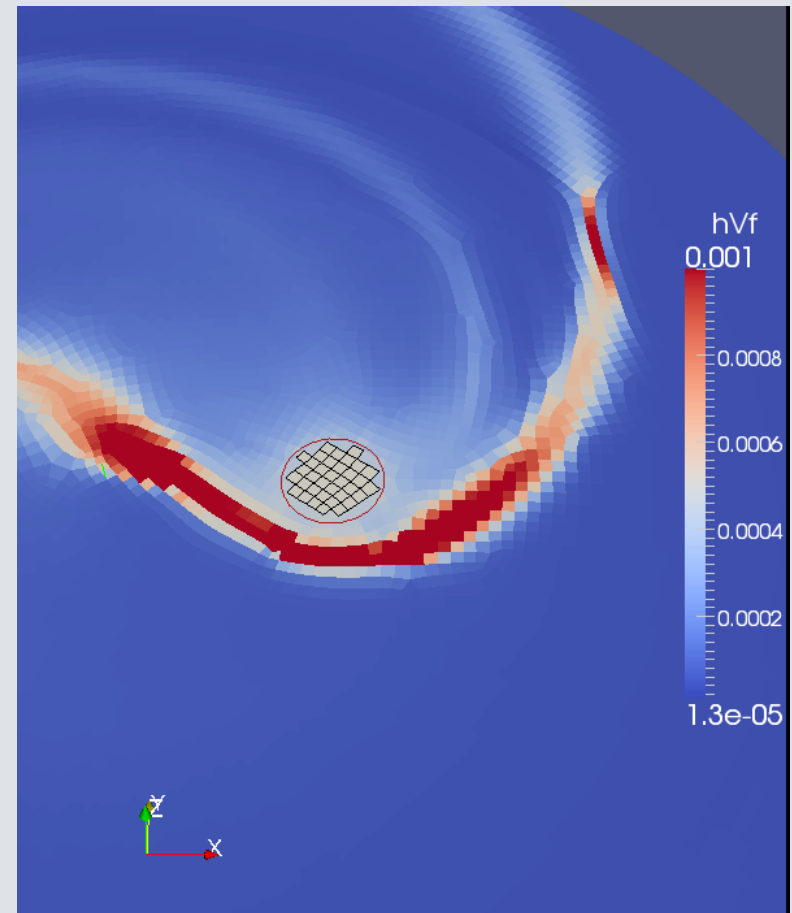
- **Solution to “Crown Cap” effect**
 - Velocity in the outer faces of the fixed area is not only determined by the location of the face centre, but also by the orientation of the edges that separate them from the free region
 - “How much fluid does the next outside face receive?”
- **Solution to total mass-flow correction**
 - Total mass-flow across edges is calculated and the velocities in the faces are normalized accordingly
- **Solution to inlet velocity profiles**
 - Simple models implemented, real data can be read-in

Impinging Jet: "Crown-Cap" Effect

Uncorrected Flow

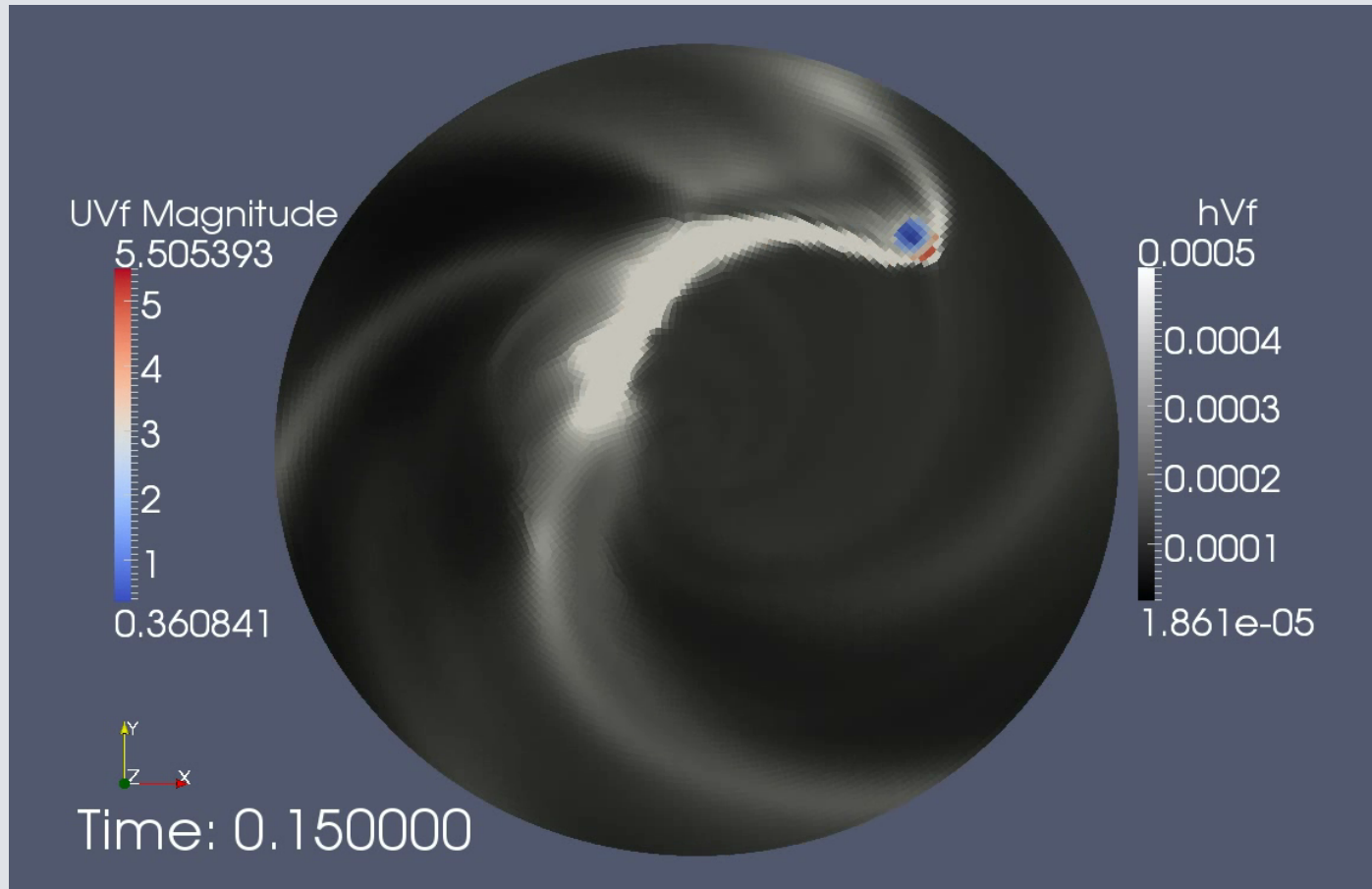


Corrected Flow



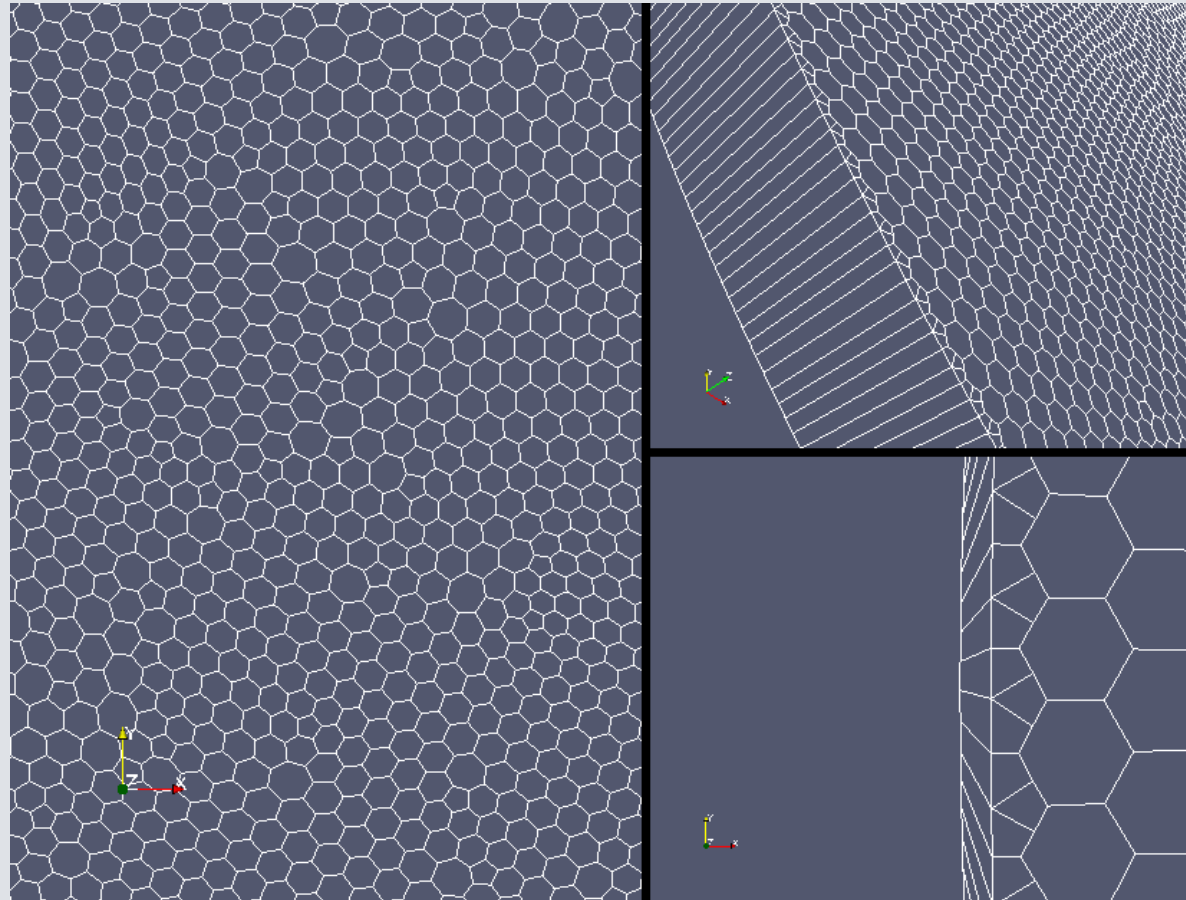
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Impinging Jet: Inlet Velocity Profile



- **Solution is very mesh sensitive**

- Mesh neutral to flow is needed to avoid artefacts
 - “flow arms”
 - “rose petals”
- Polyhedral mesh shown the best results
 - **polyDualMesh** utility used to convert a tetrahedral mesh into the polyhedral one



- **3D solution**

- Fluent software
- 5M cells, 4 CPU cores used
- 1s of process ~ 30days

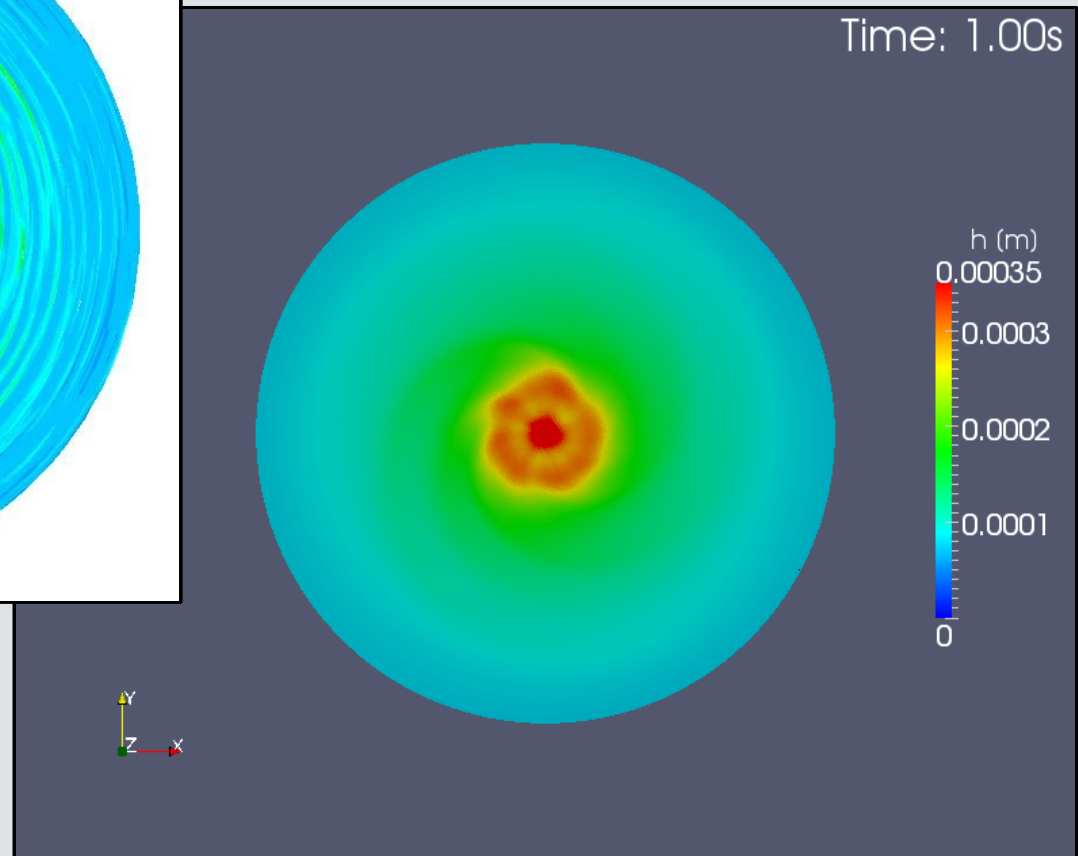
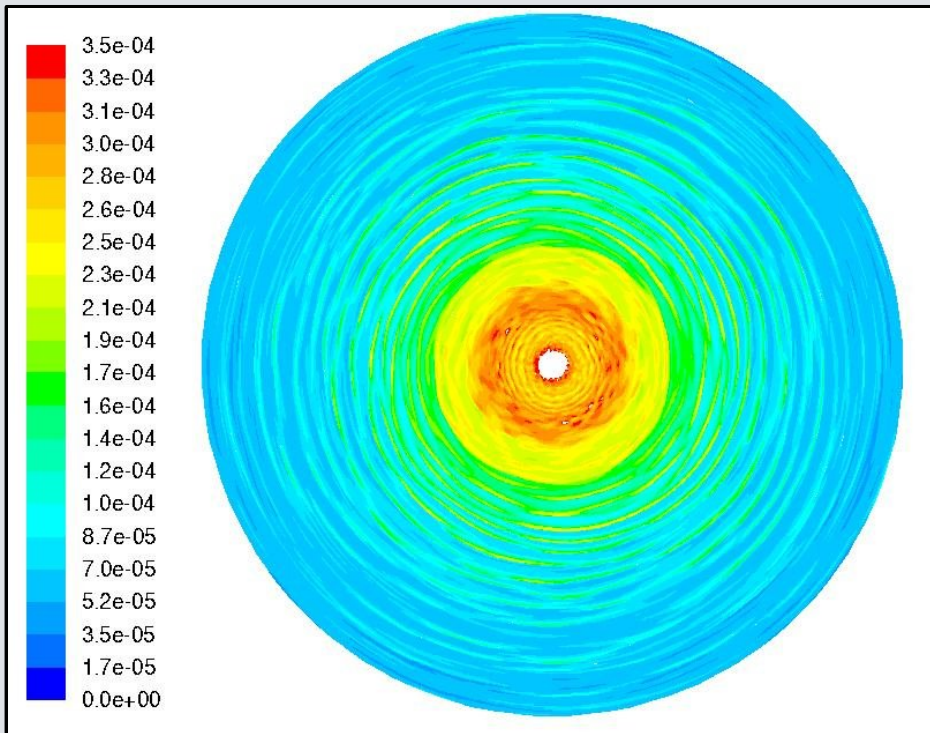
- **2.5D solution**

- OpenFOAM software
- 36.8k polydual mesh, single CPU core used
- 1s of process ~ 2hours

- **Cases**

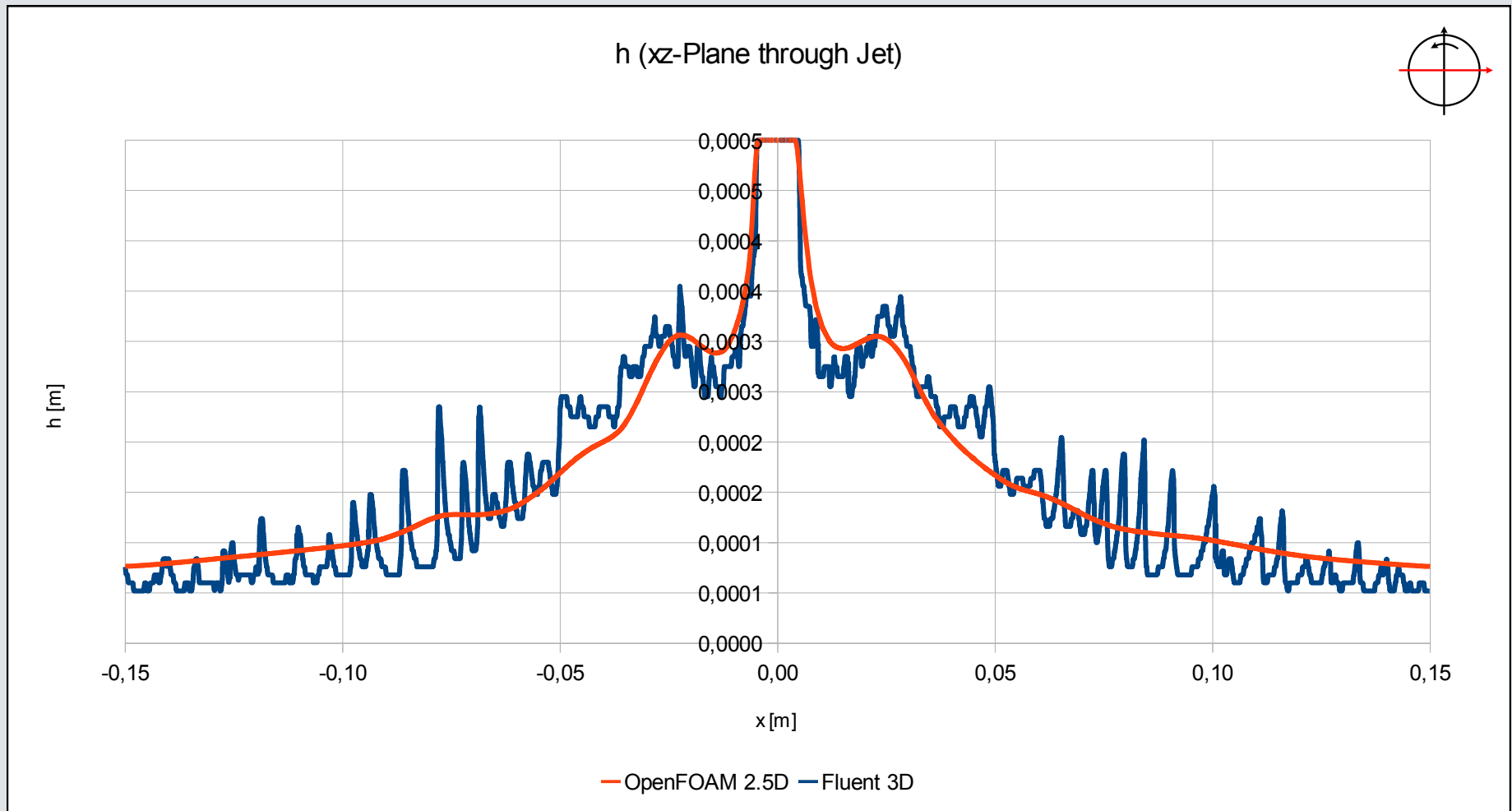
- $\Omega = 500\text{rpm}$, $Q = 1.5\text{l}$
- Spinetch-D ($\nu = 2.87 \times 10^{-6}$) or water ($\nu = 1 \times 10^{-6}$)
- Impingement area
 - Reference Case (central impingement; Spinetch-D)
 - Case 1a (ex-centric case, $\Delta r = 30\text{mm}$; Spinetch-D)
 - Case 2b (ex-centric case with dry spot, $\Delta r = 50\text{mm}$; water)
- No moving inlet was simulated

Reference Case: 500rpm, 1.5lpm, Spinetch-D

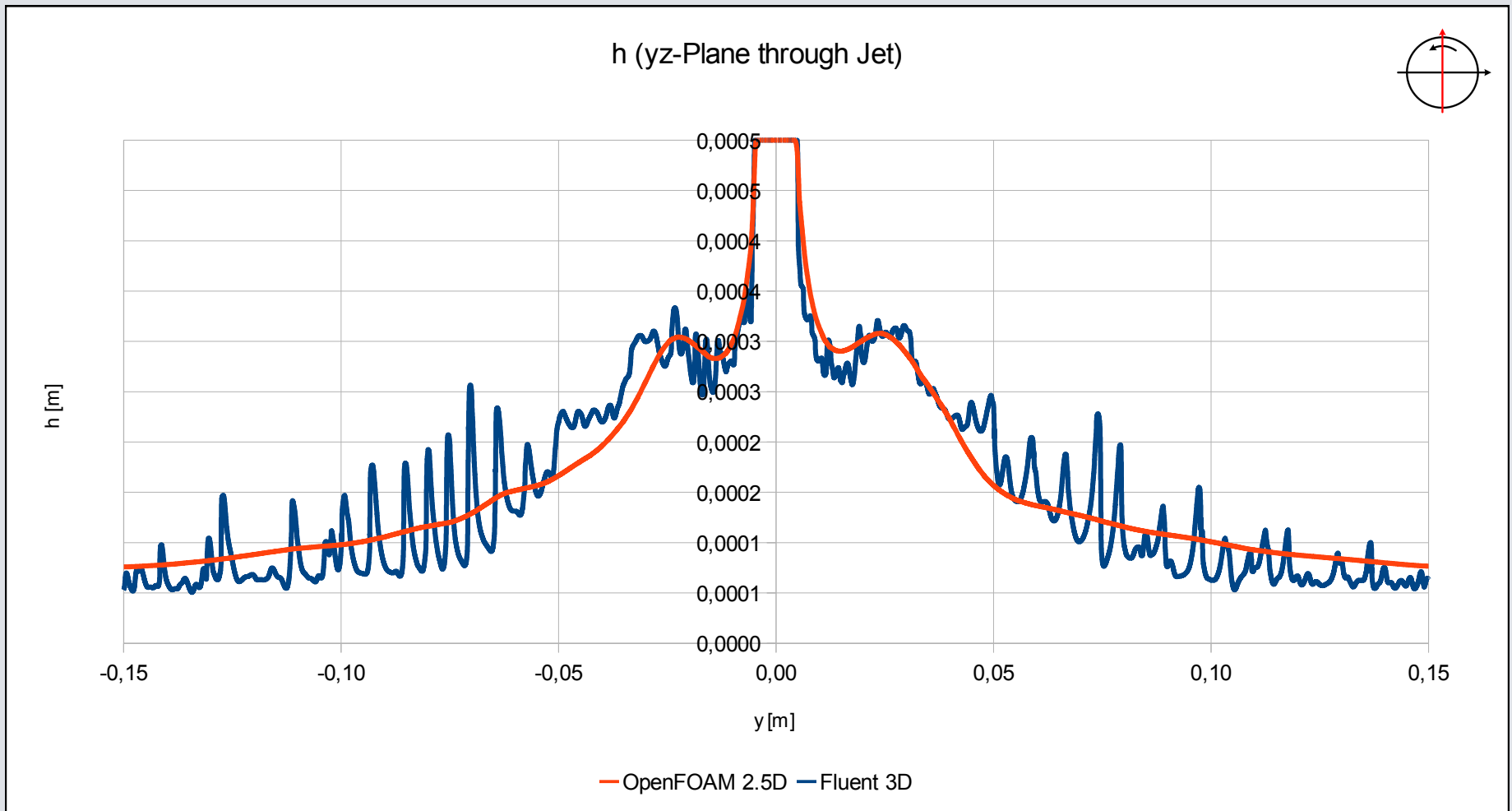


... your problems flow to a solution!

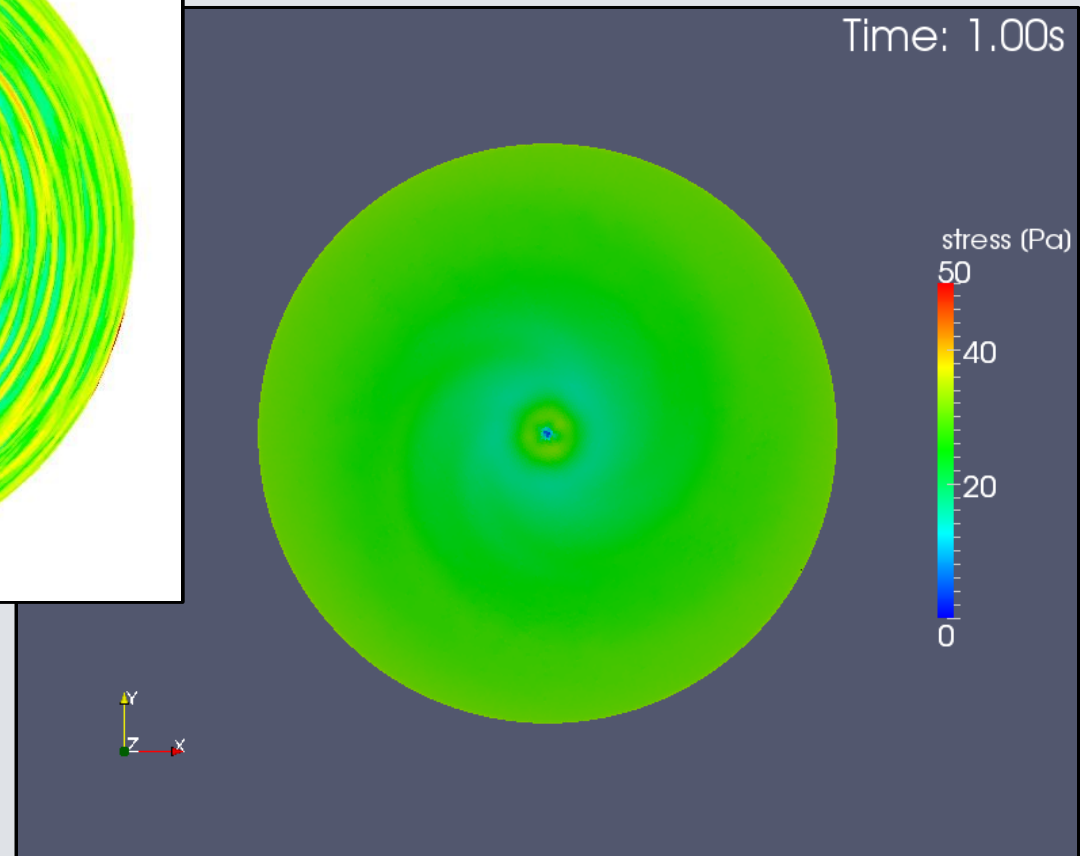
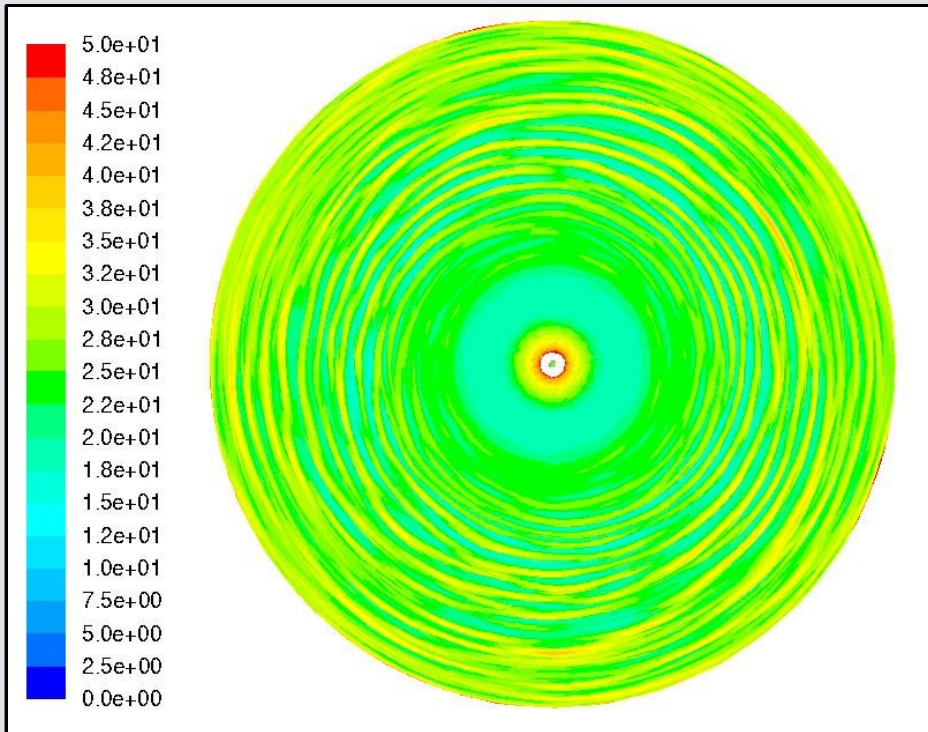
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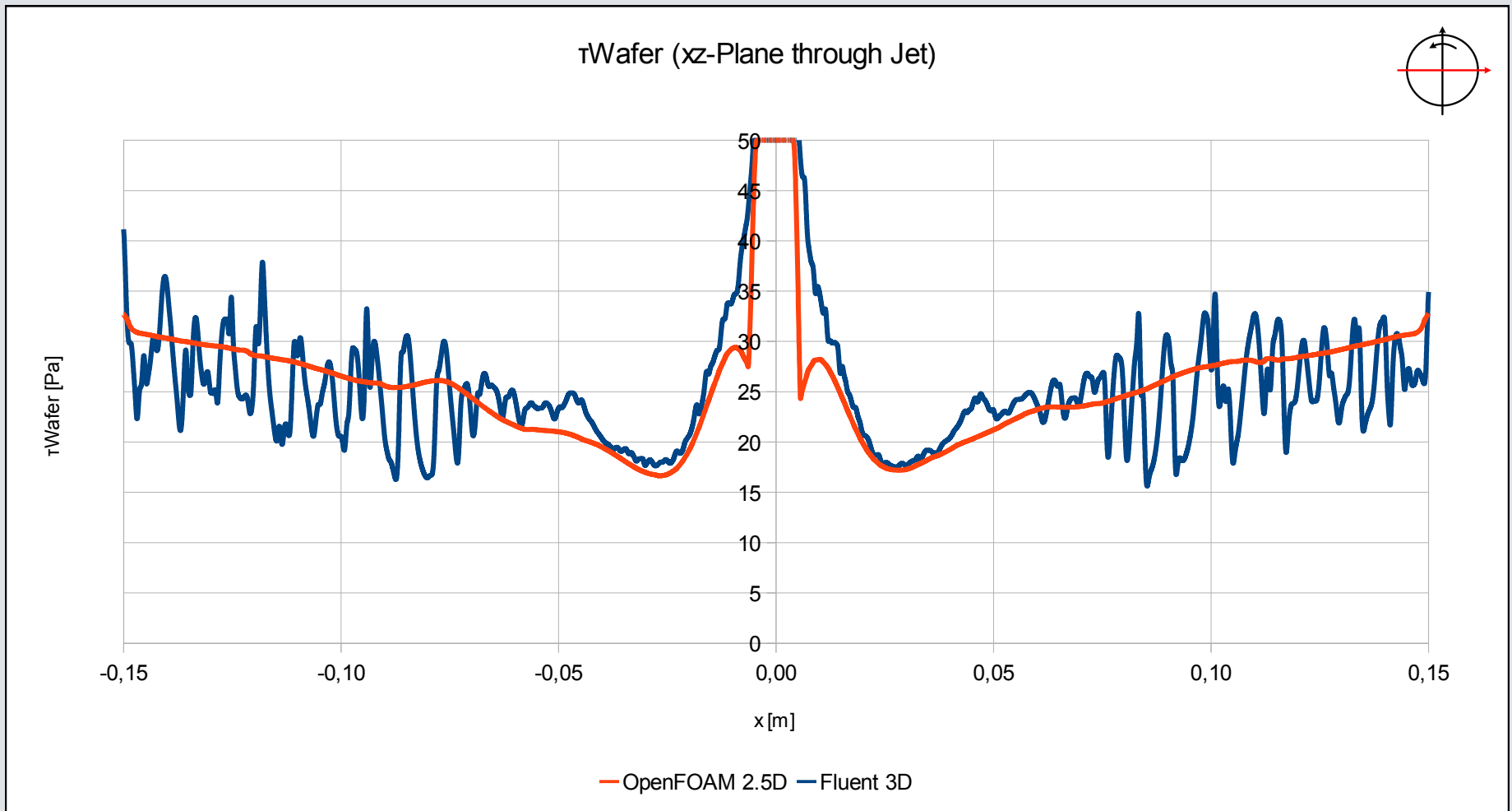


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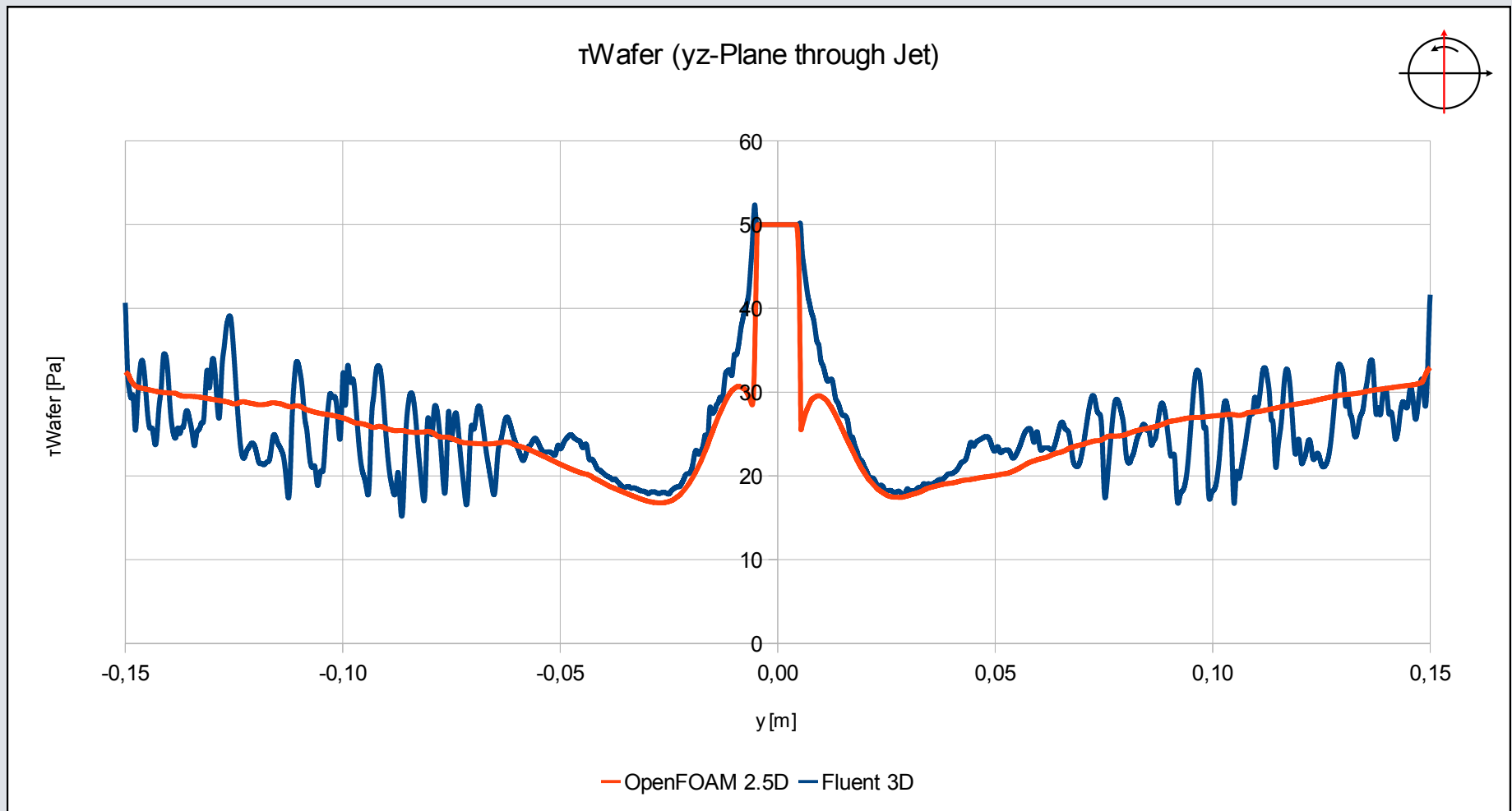


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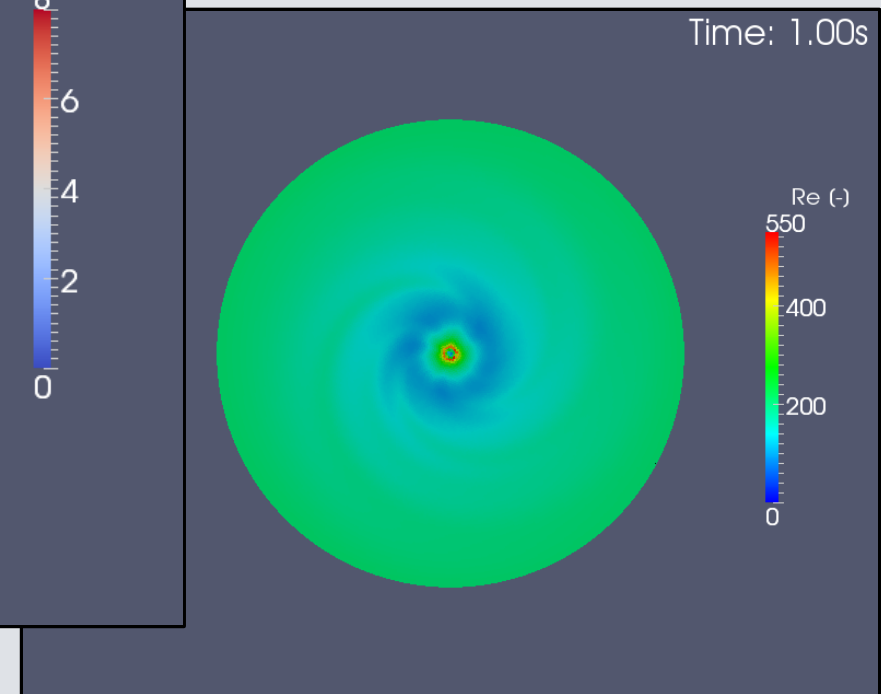
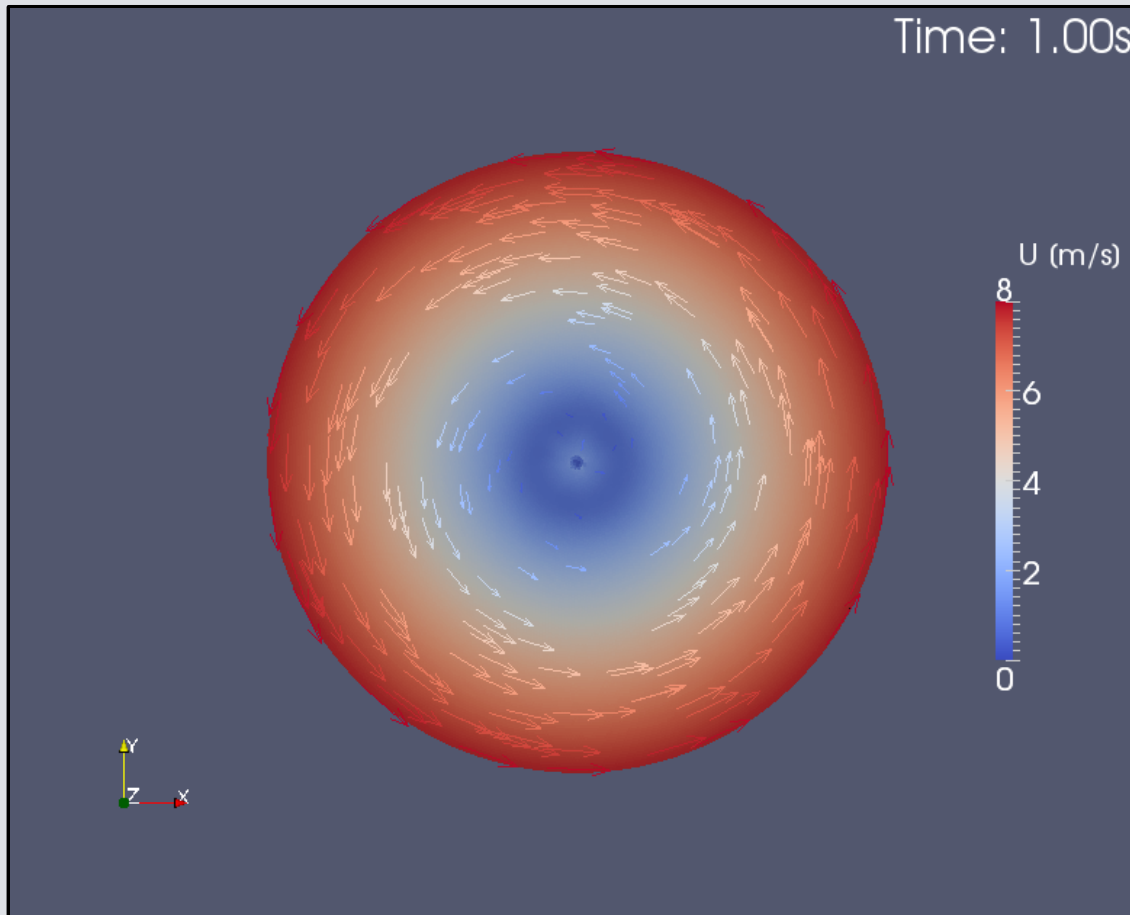
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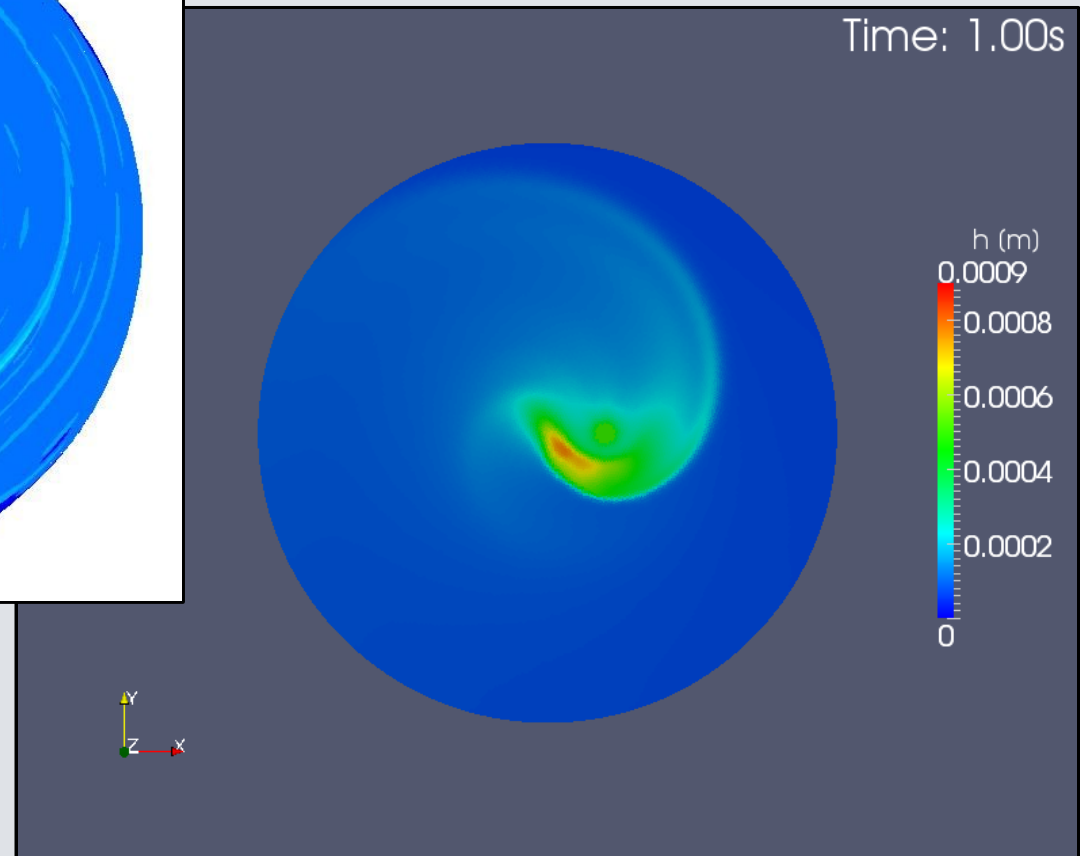
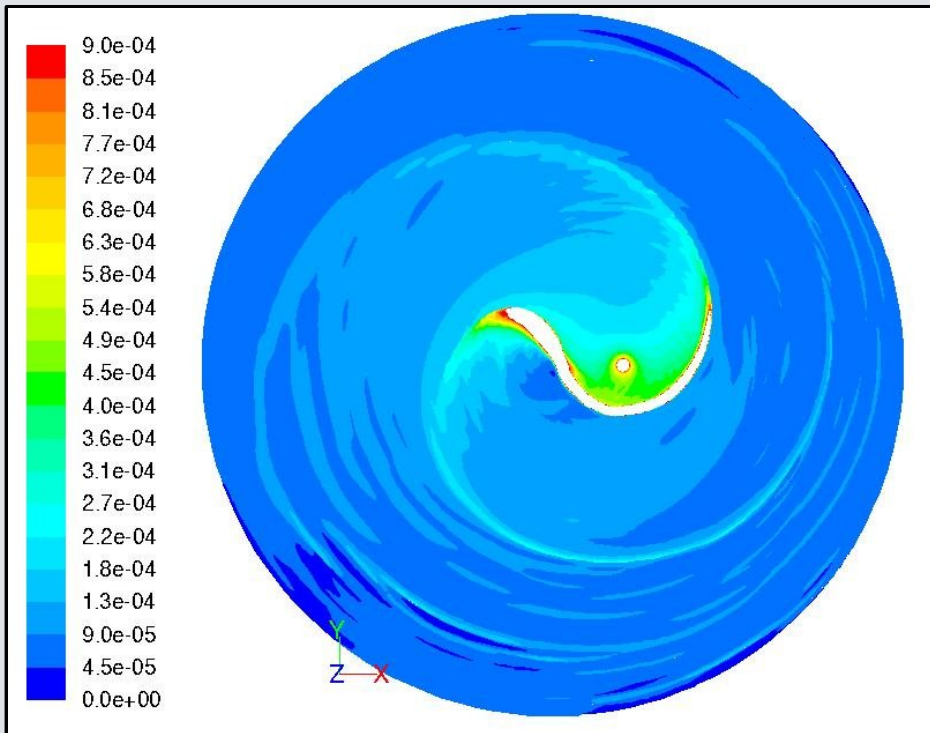


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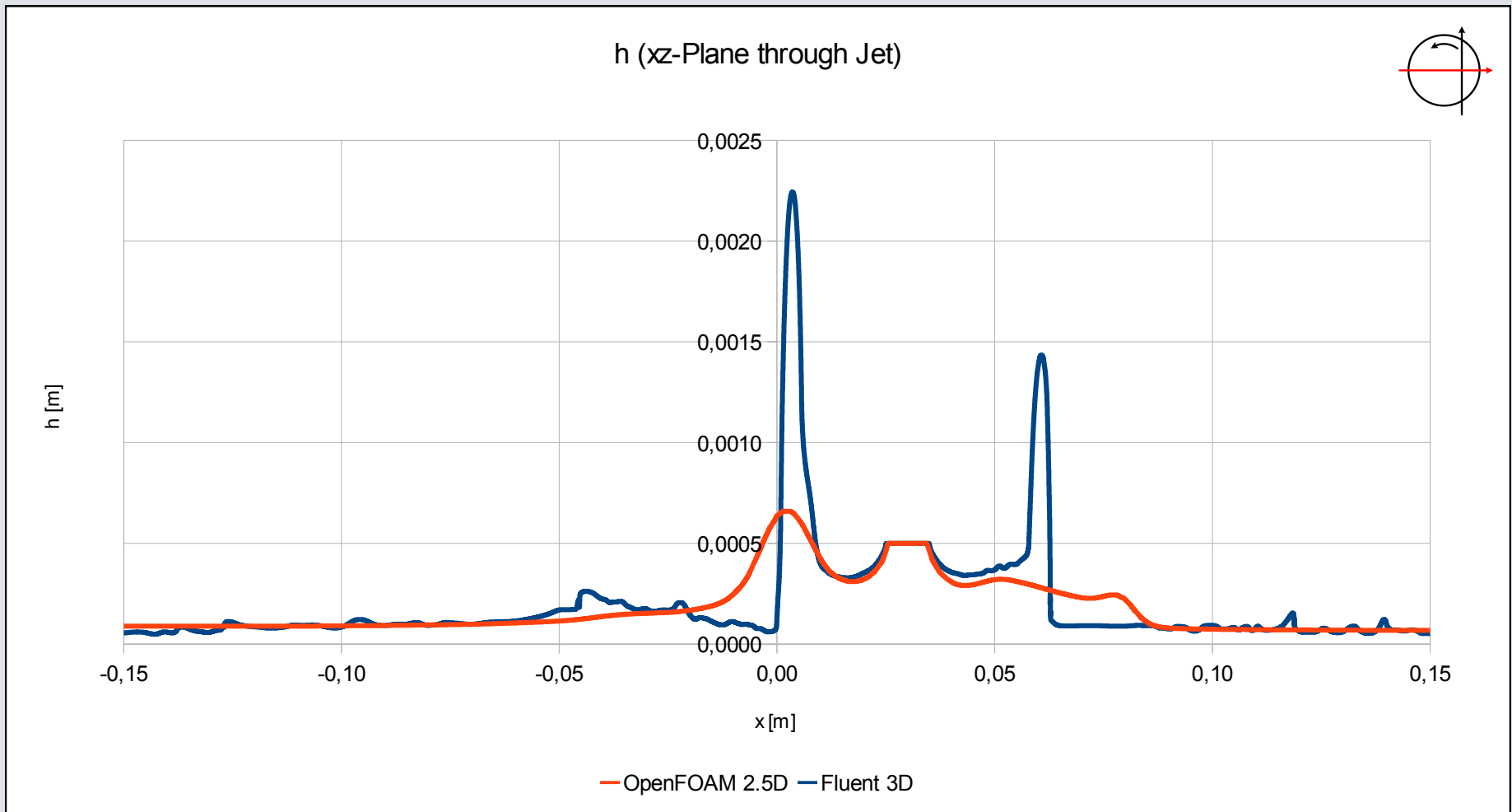
... your problems flow to a solution!

Case 1a: 500rpm, 1.5lpm, $\Delta r=30\text{mm}$, Spinetch-D

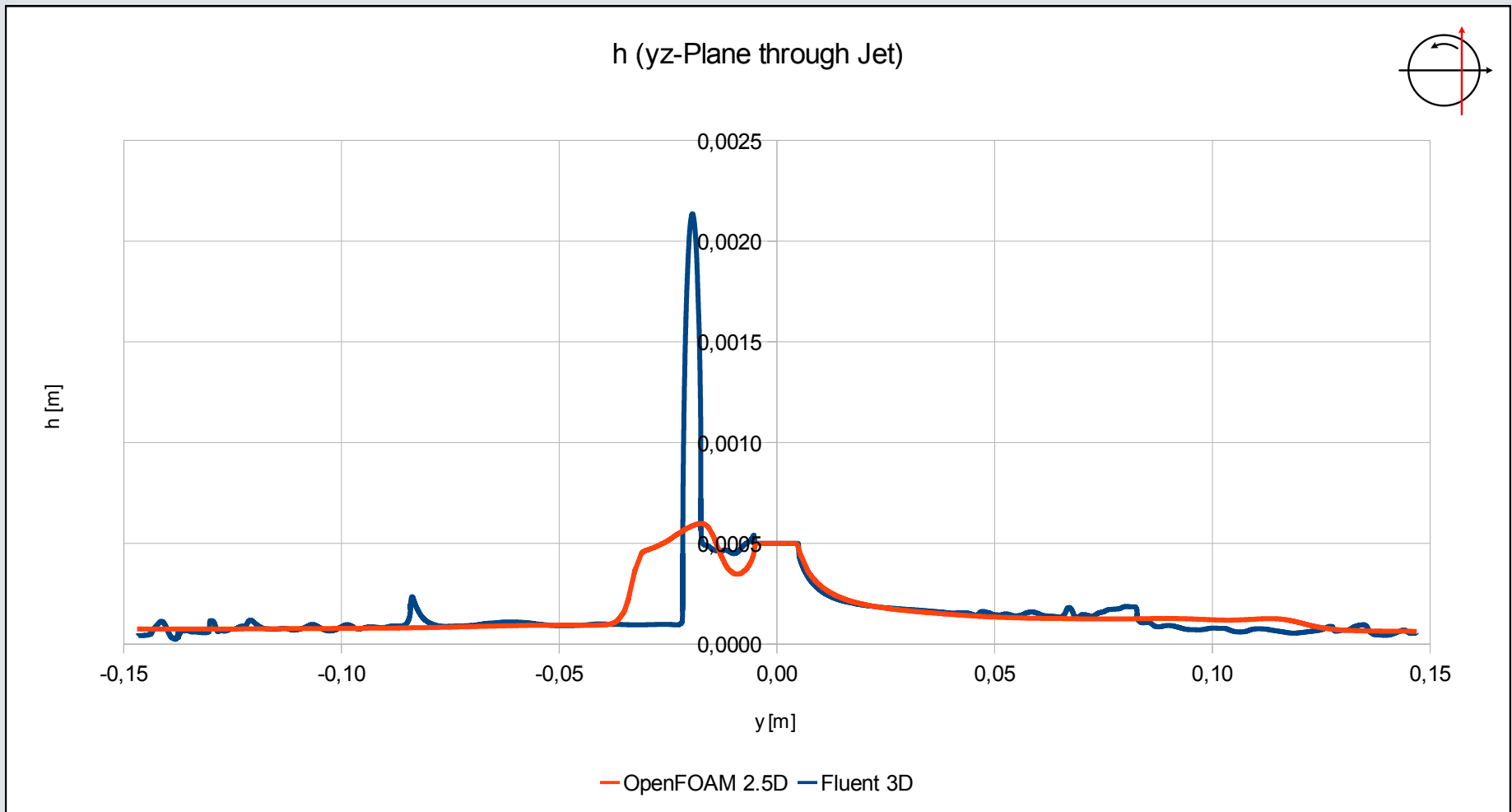


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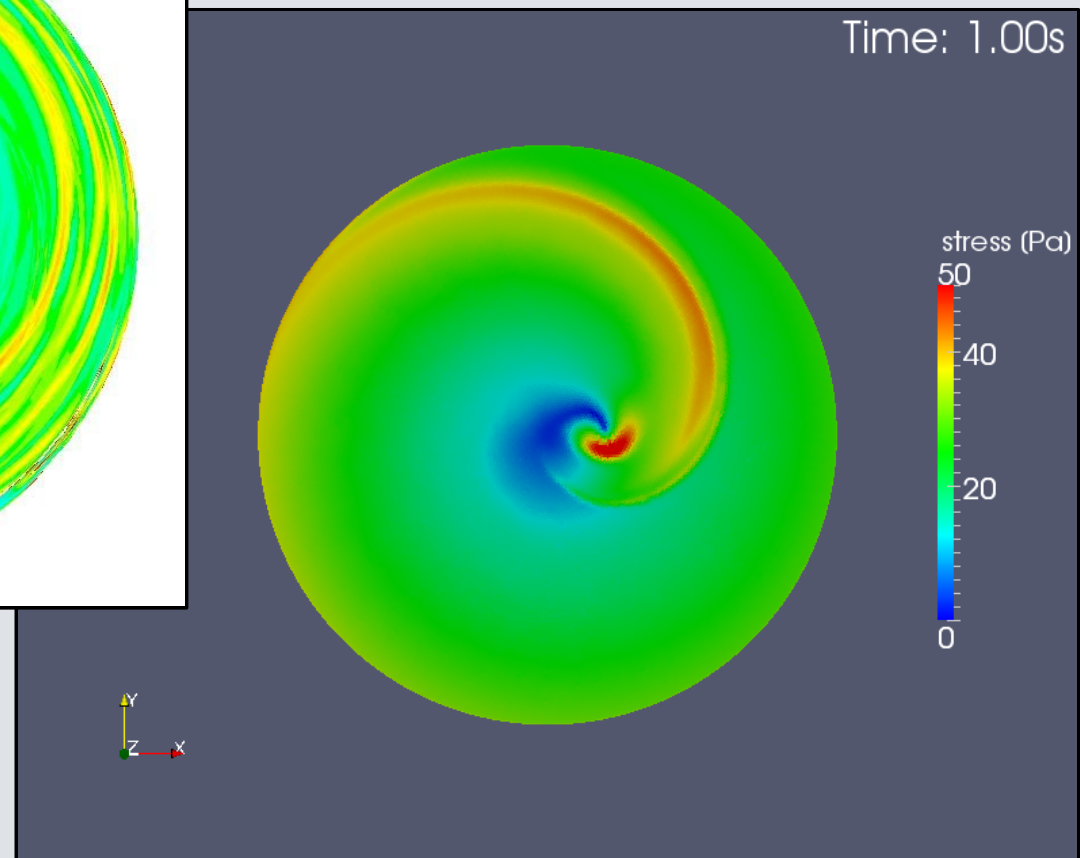
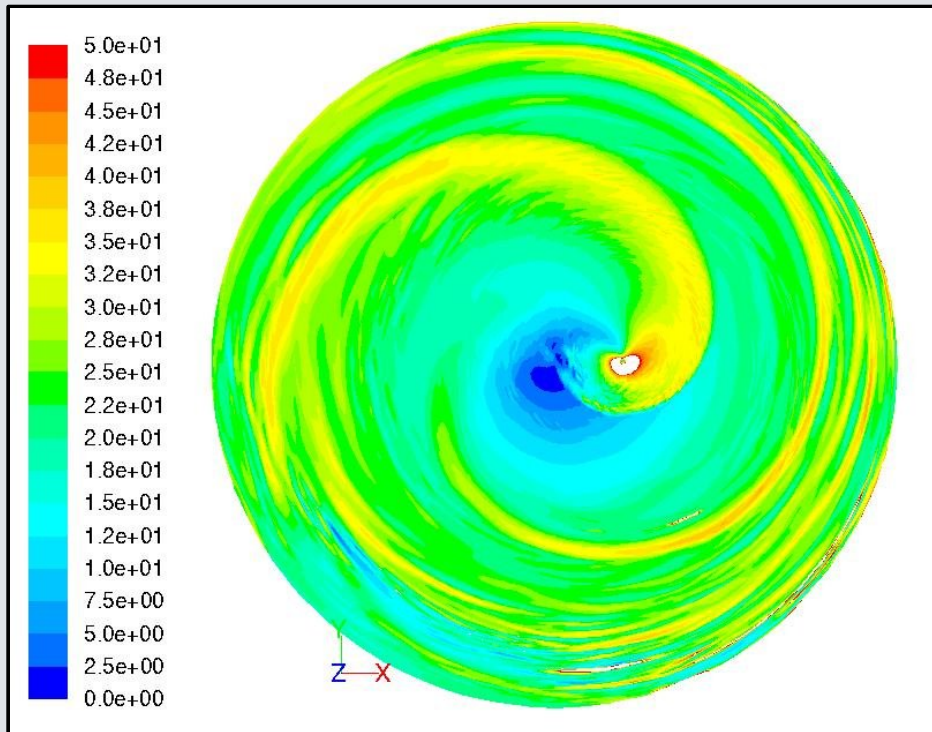
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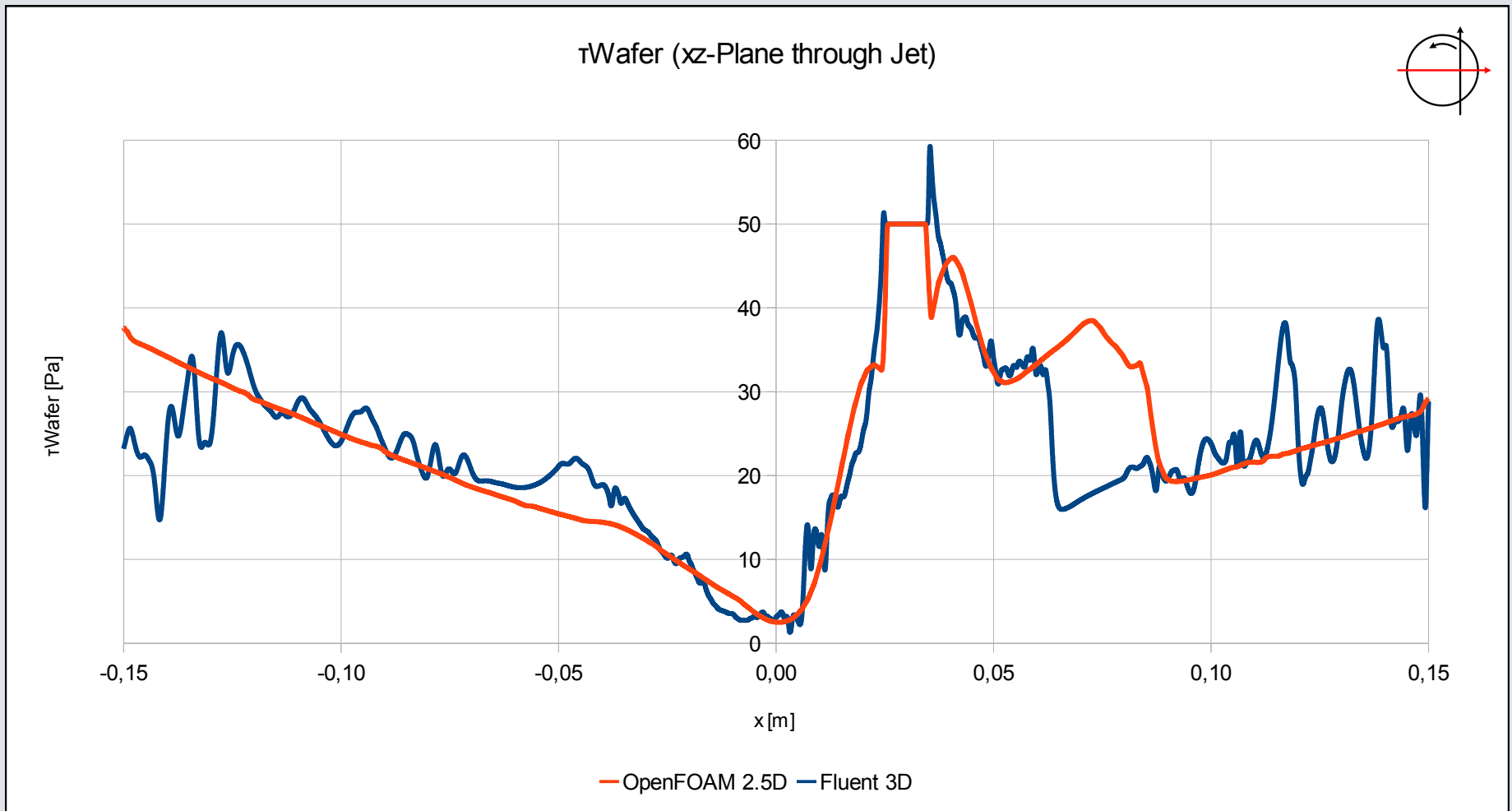


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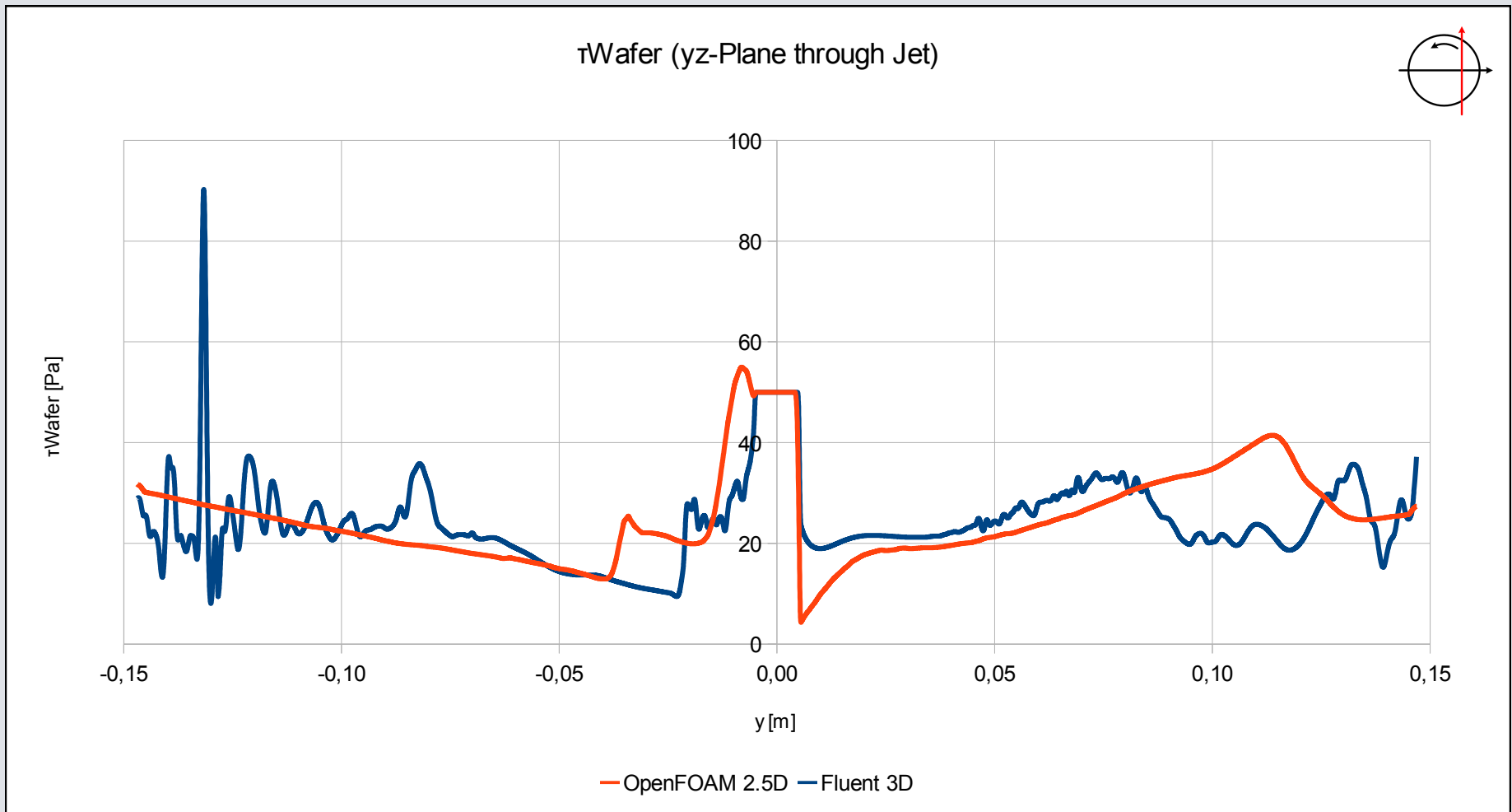


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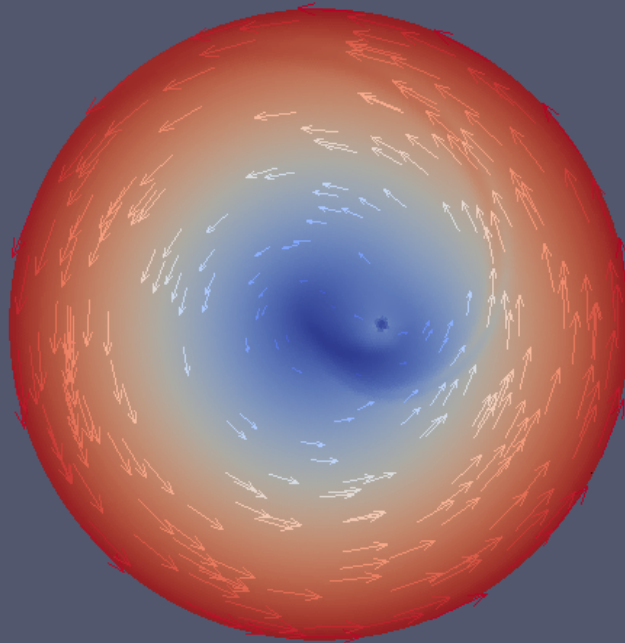


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Time: 1.00s



U (m/s)

8

6

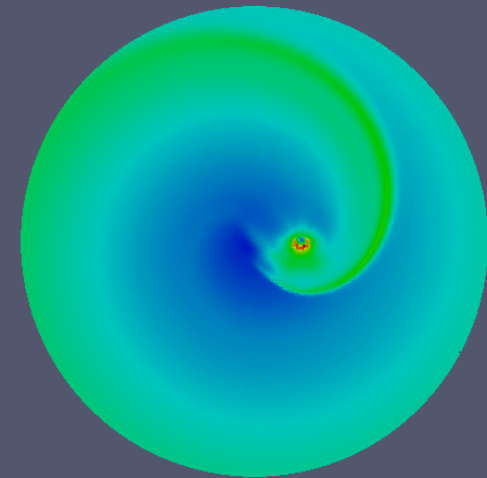
4

2

0



Time: 1.00s



Re (-)

650

600

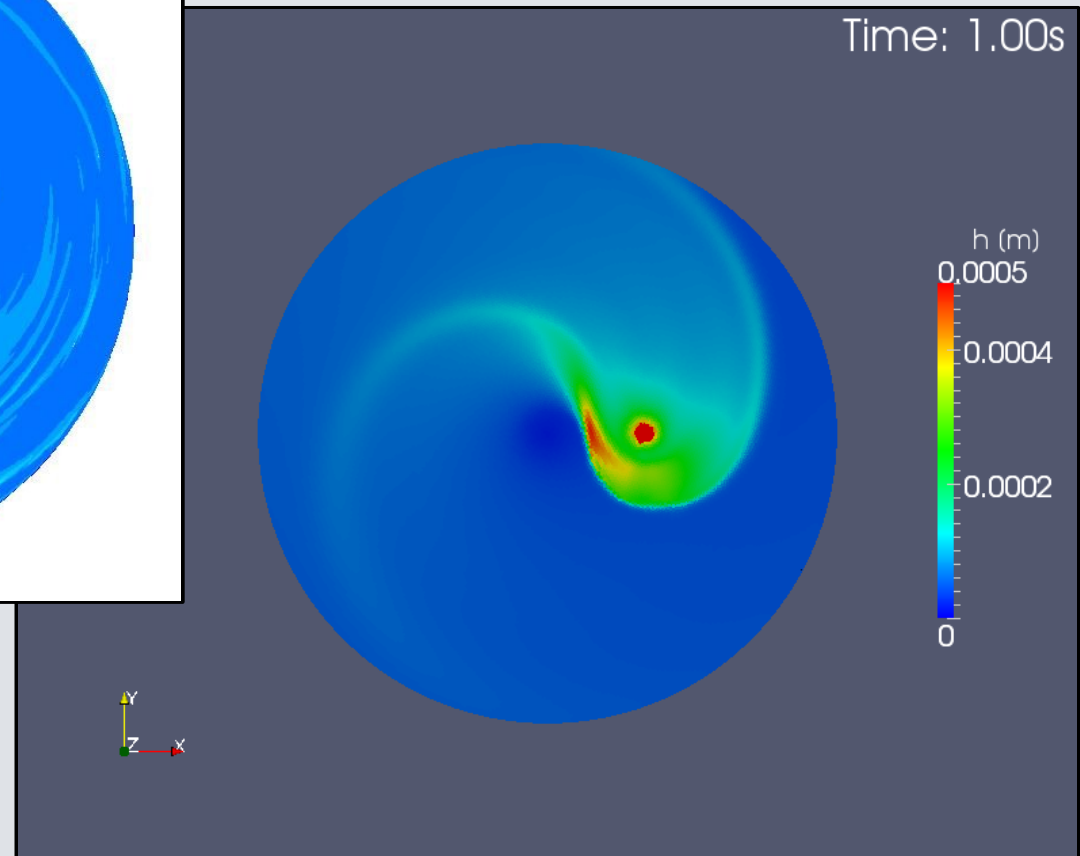
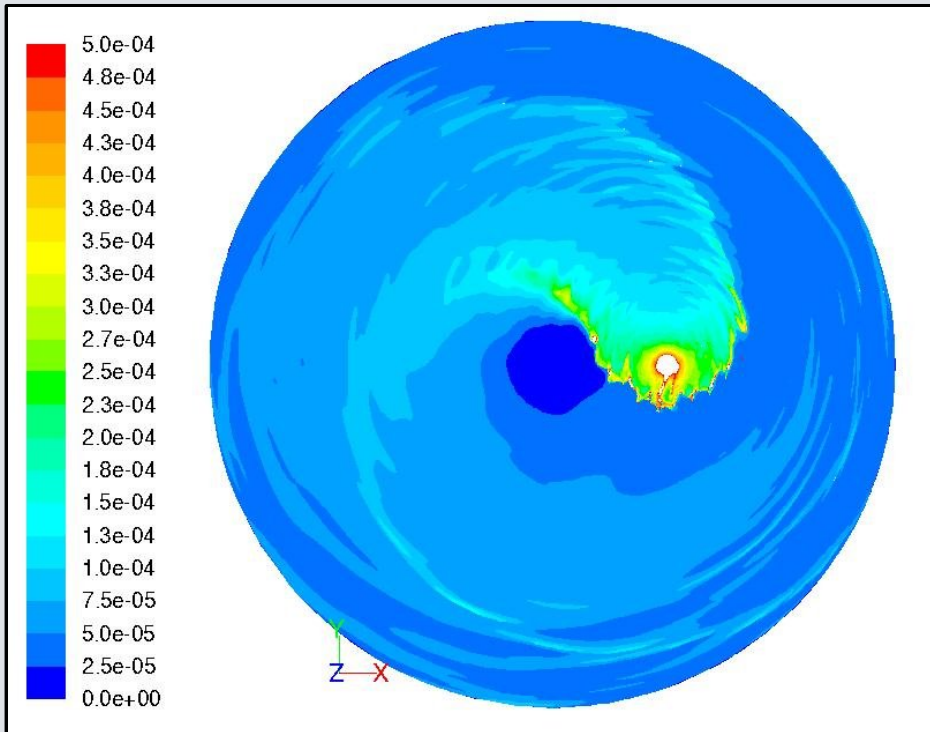
400

200

0

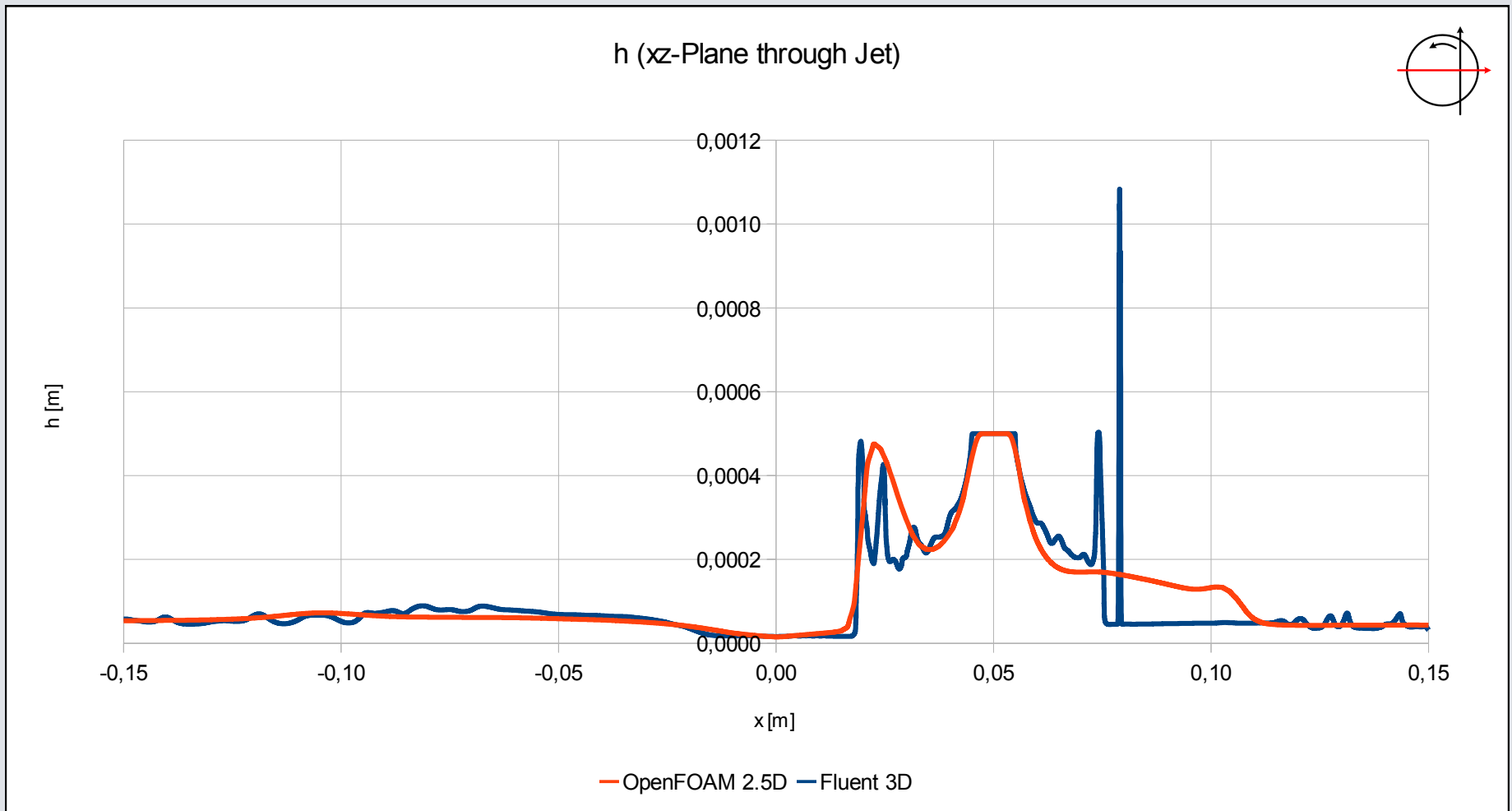
... your problems flow to a solution!

Case 2b: 500rpm, 1.5lpm, $\Delta r=50\text{mm}$, water

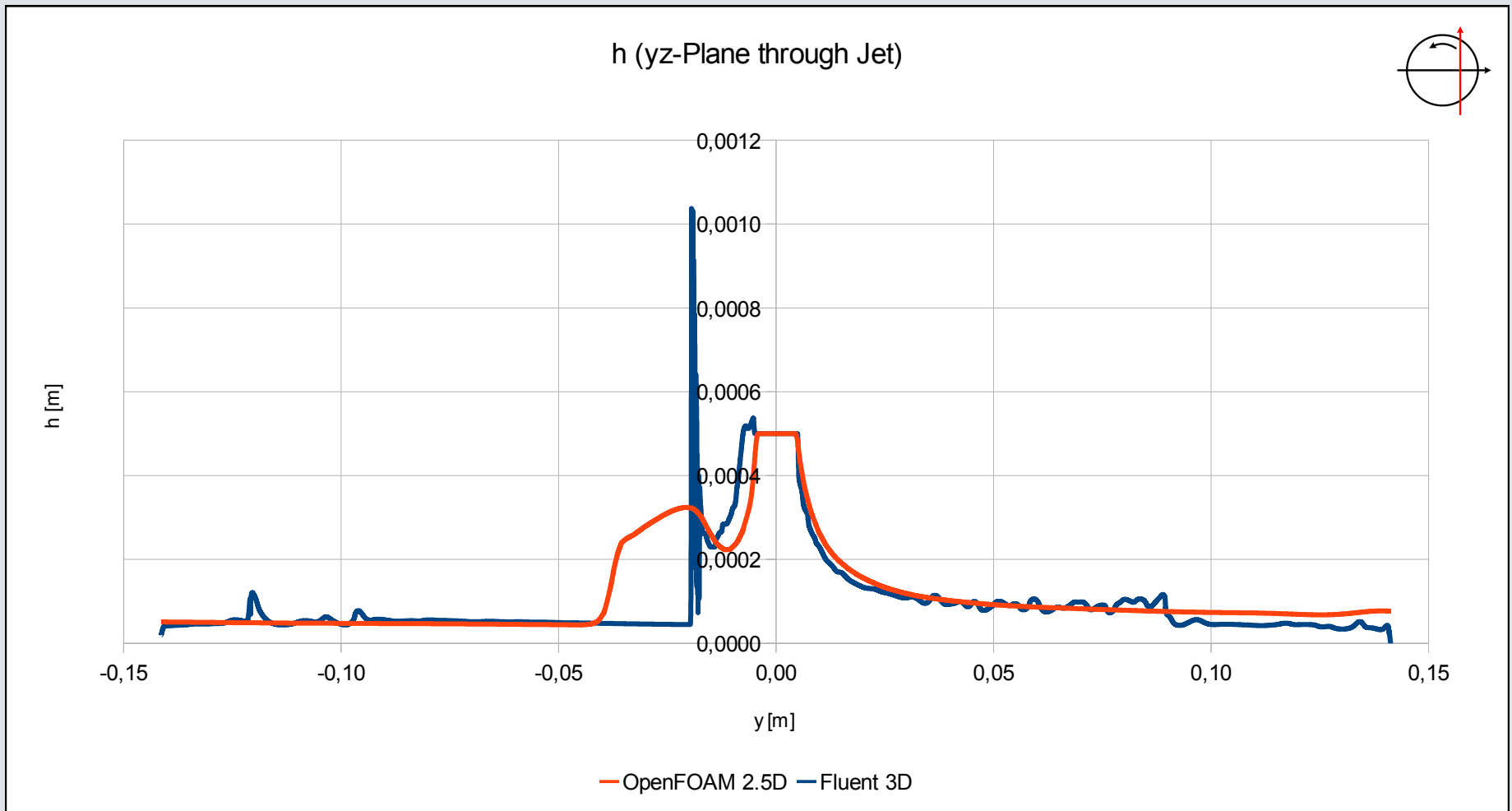


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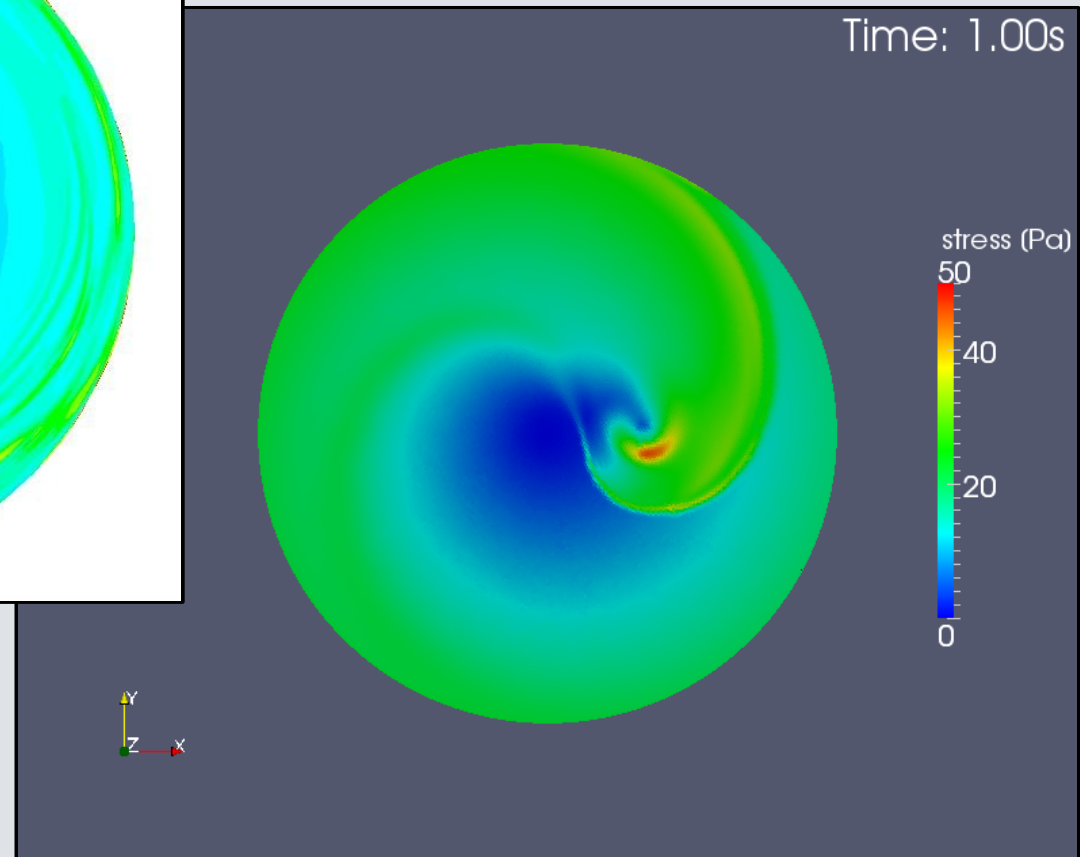
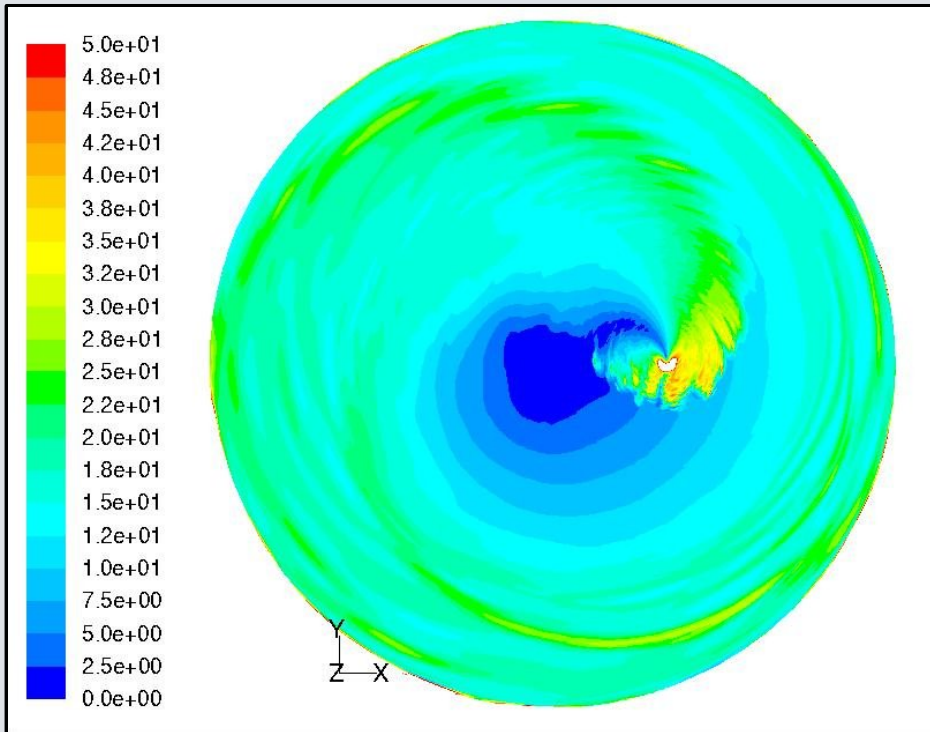
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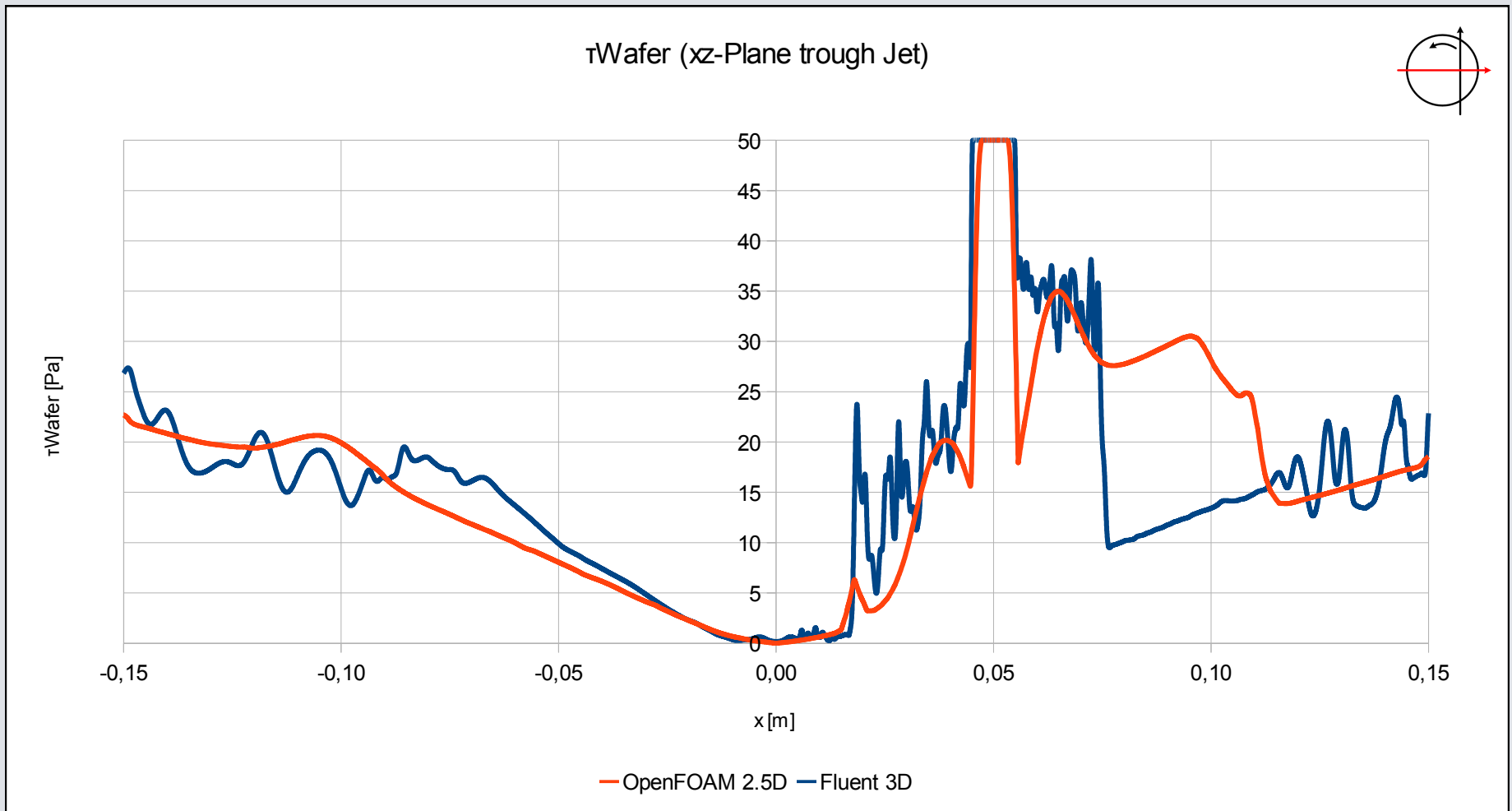


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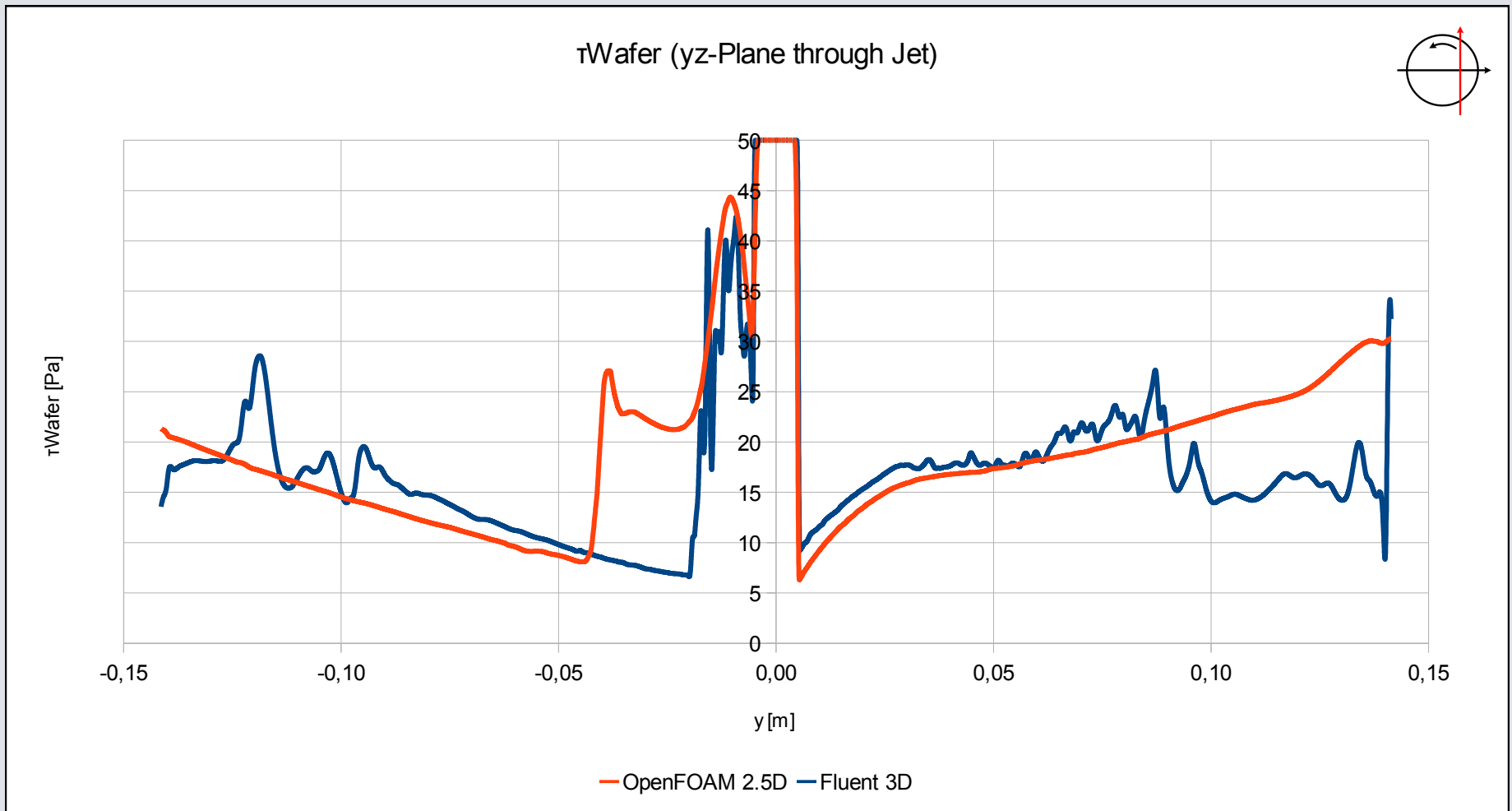


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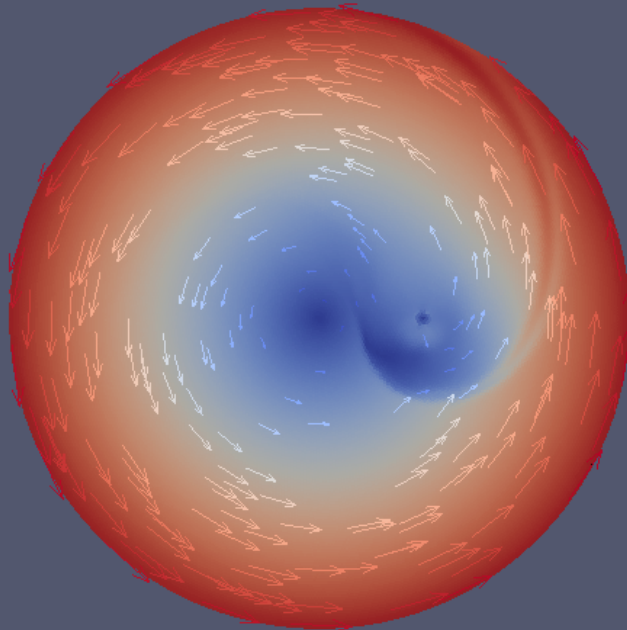


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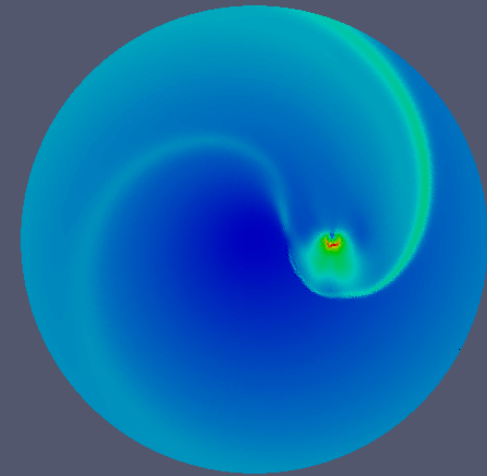
Time: 1.00s



U (m/s)



Time: 1.00s



Re (-)



... your problems flow to a solution!

- **2.5D solution shows a good agreement with 3D solution, while significantly saving on resources**
 - Solution in an impingement area has to be prescribed
 - Zone close to jet, influenced by the impingement, is showing a reasonable agreement and is still able to capture important effects
 - We never promised to be exact there!
 - Zone outside of the impingement influence is showing a very good agreement
 - Shear-stress prediction is good enough
 - Important for a chemistry reactions
 - Smooth solution without fluctuations
 - Small meshes and significantly shorter simulation times

- **Outlook**

- Dry spot handling
- Impingement area
 - Prescribing not only dependent variables, but as well the velocity profile function itself
- Velocity profile function
 - Prediction of the velocity boundary
 - Hydraulic jump modelling
 - Would be great for comparison with experiments!
- Simple etching model
 - Prediction of the concentration boundary

- **Discussion**

- Thank you for your attention! Questions?